

# Analysis of Fitting Loss Coefficient with Fitting Venturimeter in a Pipe System

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**Abstract:** Quantification of minor losses associated with a pipe fitting and regular updating is necessary for ensuring the sustainability of the system. In this study, based on simple lab based experiments, the minor loss coefficient associated with a venturimeter fitted in a pipe system is estimated. It is seen that the loss coefficient varies inversely with the increase in the Reynold’s number and can be depicted with a simple mathematical equation.

Keywords :Loss coefficient, Minor loss, Reynold’s number, Venturimeter.

## INTRODUCTION

In the flow through pipe systems, major losses and minor losses need to be accounted properly in order to supply the required energy to the flow. While major losses are due to friction, minor losses are associated with change in pipe geometry (expansion, contraction, bend etc) or fitting of valve etc. Venturimeter are most widely device for measuring discharge in a pipe system. The fitting of this device in the pipe system will cause losses and these losses will be particularly significant for a small pipe system such as that used in a drip irrigation system. It is necessary to quantify these minor losses and design the energy requirement accordingly so that sustainability of the system can be

## METHODOLOGY

In the experimental set-up, water enters the horizontal venturimeter fitted in a circular pipe of 40cm diameter. The venture consists of a converging section, a throat (of diameter 20cm) and a gradually diverging section. A differential watermanometer is fitted between the inlet pipe and the throat of the venturimeter as shown in Figure 1

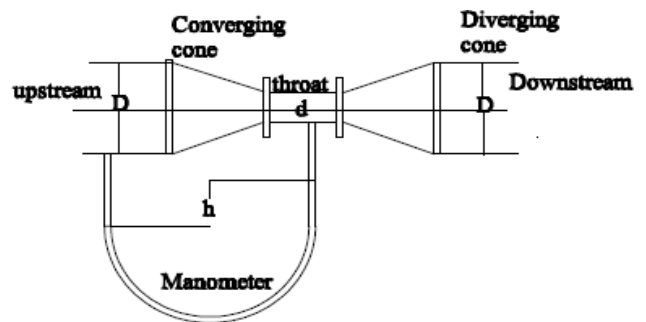


Fig. 1. Venturimeter

The overall methodology adopted is discussed as below: From the manometer fitted between the convergent section of the venturimeter and the throat, the pressure drop is estimated. Bernoulli’s equation is used to measure the head loss in this section.

ensured. Generally, the minor losses are expressed as a function of velocity head. To estimate the minor loss due to fitting of venturimeter, the loss coefficient has to be  $V^2$

$$\frac{1}{2} \left( \frac{1}{Z} - \frac{1}{Z} \right) \frac{V^2}{2g} = \frac{h}{2g} + \dots$$

(1)

estimated. There is no explicit reported work in the said objective, except a few related works. For instance, Farsirotou et al (2014) conducted experimental studies to estimate the minor losses associated with a Reynold's number indicated that for Reynold's number between 2000 to 5000, the non-dimensional number head loss (which is essentially the loss coefficient) decreased after which it remains constant within the statistical error. The current work differs from the previously reported work in the sense that a procedure for minor loss estimation associated with the venturimeter as a whole based on the experimental set-up available in fluid mechanics laboratory is proposed.

Further, the experiment has been conducted for Reynold's number upto 55000

where  $h_L$  is the head loss between the section 1 and 2. The other three terms are pressure head, velocity head and datumhead at sections 1 and 2 respectively. The head loss includes both the friction loss (major loss) as well as the minor loss associated with the fitting of the venturi meter. Since, the length of venturimeter is very small, and for the discharge range considered, it is safe to neglect the major loss without loss of accuracy. Hence the term  $h_L$  represents only the minor loss.  $p_1$  and  $p_2$  represents the pressures at the sections 1 and 2 respectively.

The velocity is estimated by measuring the discharge in the collecting tank of area 'A' for 'x' cm rise in the water level at time t. The velocity of flow, V, through the pipe is calculated by dividing the actual discharge  $Q_a$  in the pipe with the area 'A' of the pipe.

$Q_a$  is given by  $Q = Ax/t$

(2)

The head loss in the divergent section is assumed to be same as that obtained in the convergent section for a given discharge.

The total head loss ( $h_L$ ) is obtained as the sum of head loss in convergent and divergent sections.

In order to reduce the effect of experimental errors, the following steps are taken. The experiments are done in the possible wide range of discharges as per the limit of the apparatus. As many as 28 readings are taken. Since  $C_d$  is expected to be more when the discharge is high and vice versa, it is expected that loss coefficient will also vary with discharge. Further, one can obtain same  $C_d$  value for different combinations of head difference and discharge due to experimental errors. It is hence recommended to find the values of loss coefficient for average head loss and discharge combinations corresponding to  $C_d$  values of 0.97, 0.98 and 0.99.

To estimate  $C_d$ , the following equation is used

$$C_d = \frac{Q}{Q_t}$$

where  $Q_t$  is the theoretical discharge estimated as

$$Q_t = \frac{A_1 A_2}{\sqrt{A_2^2 - A_1^2}} \sqrt{2gh}$$

S.N o	Loss coefficient			
	$h_1(m)$	$h_2(m)$	$t(s)$	$Qa(m^3/s)$
1	0.62	0.28	15	8.33E-04
2	0.625	0.255	14	8.93E-04
3	0.8	0.16	11	1.14E-04
4	0.435	0.36	32	3.91E-04
5	0.568	0.305	17	7.35E-04
6	0.52	0.325	20	6.25E-04
7	0.59	0.285	16	7.81E-04
8	0.695	0.225	13	9.61E-04
9	0.57	0.3	17	7.35E-04
10	0.595	0.25	16	7.81E-04
11	0.625	0.275	15	8.33E-04
12	0.448	0.361	30	4.17E-04
13	0.625	0.272	15	8.33E-04
14	0.66	0.225	14	8.93E-04
15	0.745	0.195	12	1.04E-04
16	0.415	0.362	39	3.21E-04
17	0.44	0.365	34	3.68E-04
18	0.478	0.35	25	5.00E-04
19	0.495	0.342	23	5.44E-04
20	0.515	0.33	21	5.95E-04
21	0.605	0.282	16	7.81E-04
22	0.67	0.24	14	8.93E-04
23	0.84	0.14	11	1.14E-04
24	0.71	0.215	13	9.62E-04
25	0.55	0.31	19	6.58E-04

(3)

(4)

where  $A_1$  and  $A_2$  are the areas of pipe and throat section of venturimeter respectively. 'h' is the venture head and is calculated as the difference in the manometer reading for a water manometer.

Loss coefficient ( $K_{venturi}$ ) is then calculated from the following equation.

$K_{venturi}$

$$\frac{h_L}{V^2} = \frac{K_{venturi}}{2g}$$

(5)

□ □

A graph is plotted between the non-dimensional number  $K_{venturi}$  and the Reynold's number and equation is fitted to explain the variation. For more details on venturimeter, the readers are referred to standard text books in Fluid Mechanics[F.M. White (2011), J.M. Cimbala and Y.A. Cengel (2014)]

**ESULT**

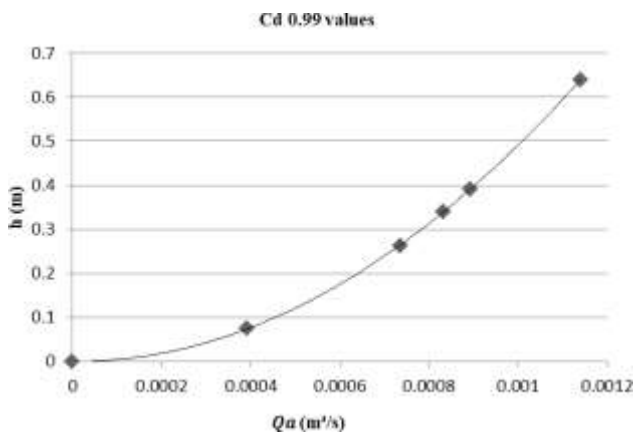
**AND DISCUSSION**

A total of 28 readings are taken involving measurement of mass flow rate and the differential pressure. The values of  $Q_a$ ,  $Q_t$  and  $C_d$  (coefficient of discharge) are also calculated. As expected, it is seen that same  $C_d$  values are obtained for different combinations of discharge and pressure head differences. The readings corresponding to  $C_d$  values of 0.97,

0.98 and 0.99 are collected together and plotted as graphs between the discharge and the pressure head difference. A best fit curve is fitted through each of these graphs from which values are read for a uniform interval of  $Q_a$ . Table I shows the reading obtained, and a typical best fit curve corresponding to  $C_d$  of 0.99,  $C_d$  of 0.98 and  $C_d$  of 0.97 is given in Figure 3, 4 and 5

**TABLE- I: DISCHARGE VARIATION WITH RESPECT TO PIEZOMETRIC HEAD**

S.N o	Loss coefficient			
	$h_1(m)$	$h_2(m)$	$t(s)$	$Q_a(m^3/s)$
1	0.515	0.325	20	6.25E-04
2	0.412	0.113	41	3.05E-04
3	0.468	0.355	26	4.81E-04



**Fig. 2.Consolidated graphical representation for Cd 0.99**

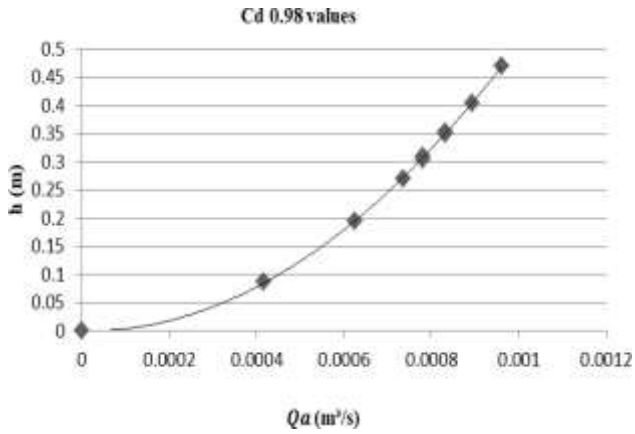


Fig. 3.Consolidated graphical representation for Cd 0.98

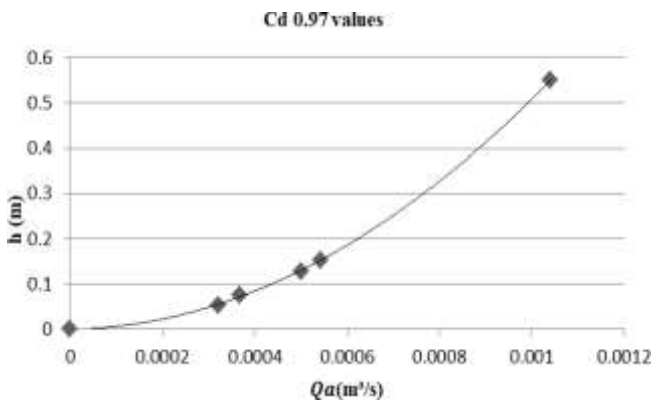


Fig. 4.Consolidated graphical representation for Cd 0.97 **TABLE- II: VENTURI LOSS COEFFICIENT FOR DIFFERENT FLOW CONDITIONS**

Data	Minor Loss	
	$Re$	$K_{venturi}$
1	16821.31	0.792399
2	19874.42	1.261548
3	23457.85	1.016904
4	28078.18	0.758335
5	36514	0.710016
6	45756.23	0.358255
7	54329.12	1.192663

Table II shows the loss coefficient values corresponding to the associated Reynold’s number presented in the order of increasing Reynold’s number. Considering the statistical error associated with the experiment, it is desired to plot the variation of average Reynold’s number in the range 15000 – 18000, 18000 – 20000, 20000 – 24000, 24000 – 30000, 30000 – 40000, 40000 – 50000 and 50000 – 60000 and with the average loss coefficient values.

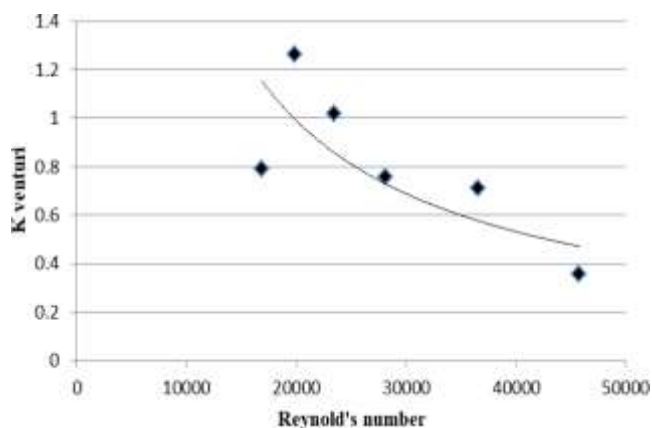


Fig. 5.Variation of Venturi loss coefficient and Re.

Figure 6 shows the plot. At Reynold’s number less than 19000, there is an increase in loss coefficient and as Reynold’s number increases beyond 20000, the loss coefficient is found to decrease. A best fit line is fitted to obtain the approximate equation as shown below

$$K_{venturi} = 6943 R_e^{-0.89} \tag{6}$$

Where Re is the Reynold’s number

It can be seen that the loss coefficient for the venturimeter is not a constant. It varies with discharge and as the discharge increases (i.e. Reynold’s number increases), the loss coefficient decreases. It is to be noted that the assumption of same head loss in the divergent section of the pipe will introduce some error. The equation 6 is valid for Reynolds number range from 15,000 to 60,000

CONCLUSION

The fitting of the venturimeter in the pipe system will incur some minor losses. The venturi loss coefficient corresponding to this minor loss is estimated and is found to decrease with the increase in the discharge or Reynold’s number. It is recommended that any pipe system fitted with venturimeter should be regularly calibrated for loss coefficient so that the sustainability of the system can be better ensured. The method suggested in this paper is an approximately method involving assumption on pressure variation from throat of venturimeter to the downstream pipe. More elaborate studies can be done the actual and accurate measurement.

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